

Thermally enhanced remediation

In Situ Thermal Desorption

Tom Heron

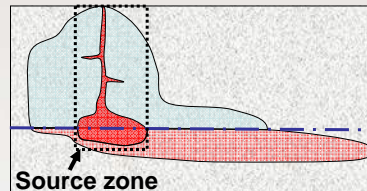
Division Director, geologist



1050 colleagues
250 environmentalists

Important tools in the toolbox

- Heavily contaminated **source zones**
- Stringent remediation requirements
- Fast clean-up
- Large volumes
- Clay/silts/fractured
- Deep contamination
- Many contaminants and mixtures



Treatable contaminants

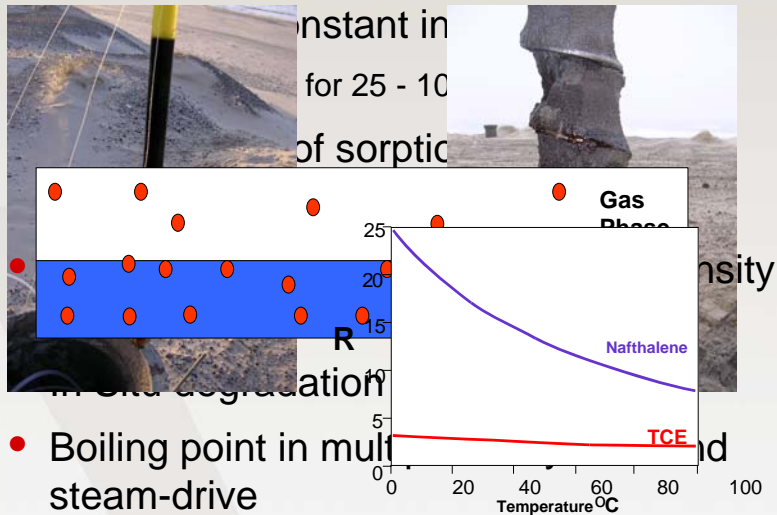
- Chlorinated Ethenes
- Oil products, BTEX
- Coal Tar
- Creosote
- PAH's, Naphthalene
- PCB's
- Chlorobenzenes
- Pentachlorophenol (PCP)
- Dioxins
- Mercury
- Many pesticides
- Mixtures

Data on much of this in
NIRAS' and Krügers
booth up stairs!!

Remediation Mechanisms

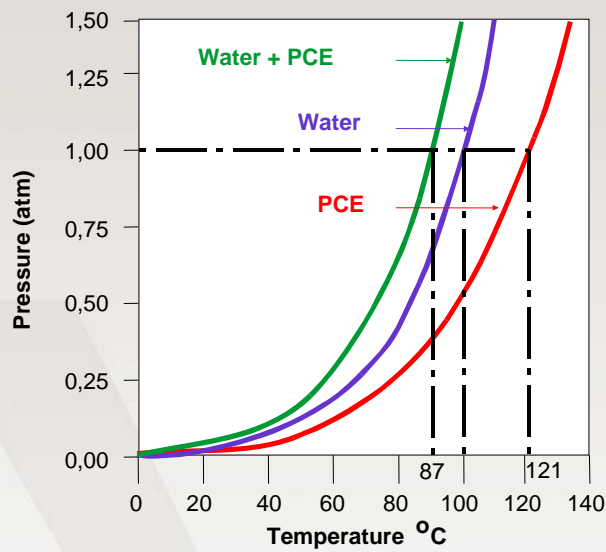
Mechanisms and values for TCE

- Vapor pressure increases
 - TCE: 18 times for 10 - 100 °C



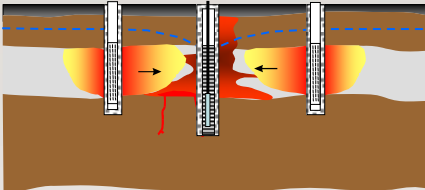
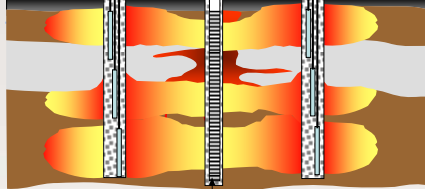
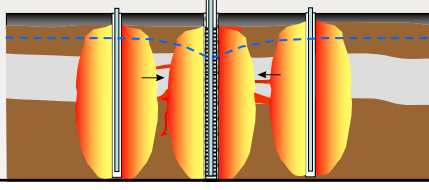
- Boiling point in mult
 - steam-drive

Boiling point in a two phase system

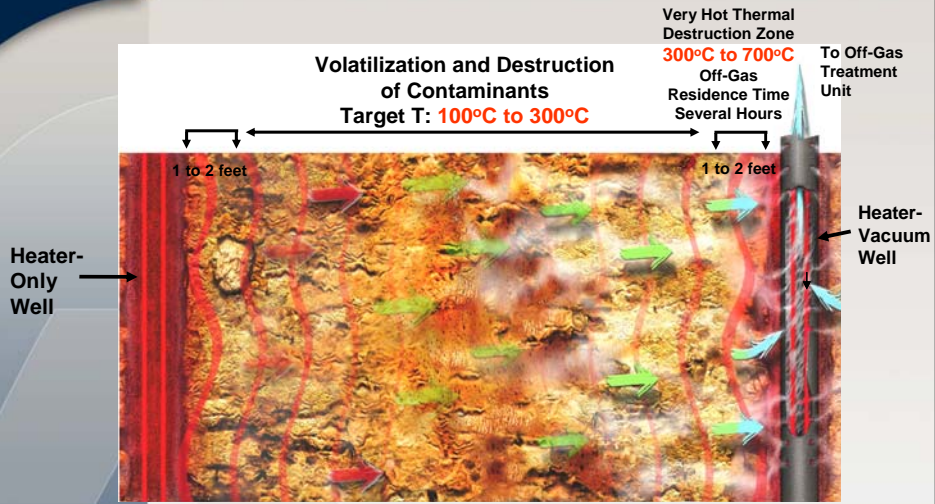


Technologies

NIRAS Important Heating Technologies - Summary

Steam	SEE - heating governed by hydraulic conductivity – non-uniform steam flow	
Electrical	ERH - heating governed by electrical conductivity	
Conductive	ISTD/TCH - heating governed by thermal conductivity – nearly uniform distribution of heat	

In Situ Thermal Desorption and destruction



Important design issues:

Important design issues

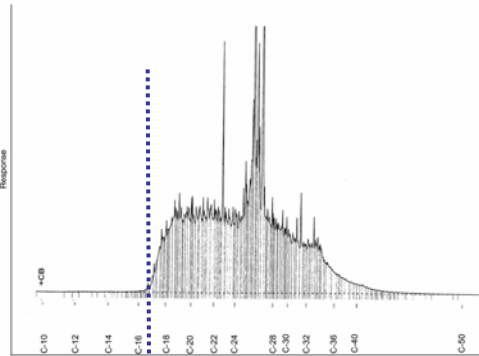
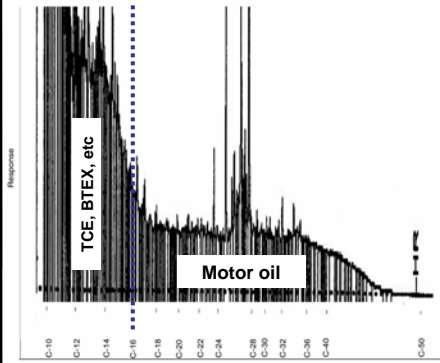
- Goals / effect on risk or value
- Time
- Price
- Liquid and vapor capture
- Condensation fronts
- Boiling water is expensive
- Temperature distribution
- Energy balance
- Organic rich soils
- Underground utilities / buildings etc.

Examples of completed projects

Goal: MCL in soil and groundwater for BTEX og chlorinated solvents
TCE: 2 mg/kg og 5 µg/l

Typical chromatogram:
Soil before Steam

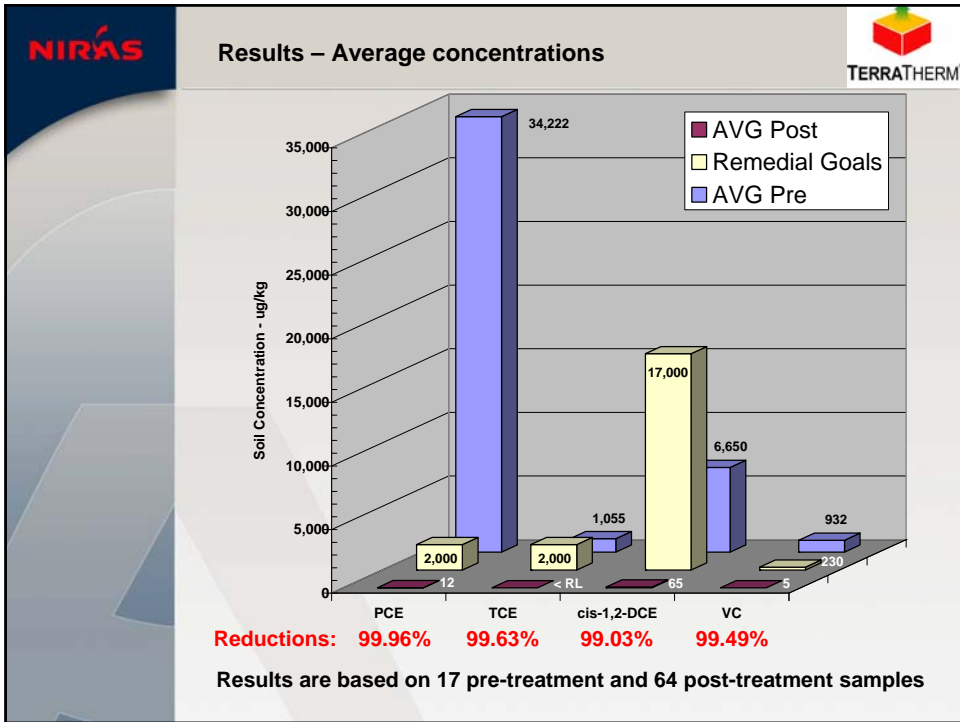
After thermal treatment



Courtesy of Kent S. Udell

UC Berkeley



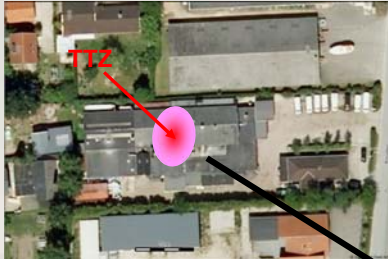


NIRAS

Ongoing Danish Projects

Knullen – Odense, Denmark

Worlds first thermal remediation using a combination of steam and ISTD



COC's: PCE, chlorinated solvents (800 kg)
 Soil: Clay and sand
 Treatment interv.: 3 – 14 m.b.g.
 Area: 240 m²
 Volume: 1.900 m³
 Estimated cost: 15 mio. dkr



Number of HV-borings: 45
 Steam injection wells: 5
 Steam extraction wells: 2
 All wells installed under a building



Skuldelev – Denmark

Full-scale design based on results from pilot test



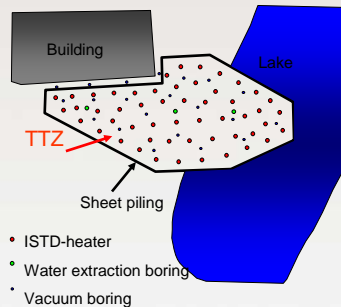
Pilot test, Skuldelev

COC's: PCE, chlorinated solvents (4000 kg)
 Soil: Clay and sand
 Treatment depth: 7,5 meters
 Area: 250 m²
 Volume: 1.600 m³
 Estimated cost: 12 mio. dkr

ISTD-wells: 53
 Vacuum wells: 21
 Water extraction wells: 3



Monitoring well, Skuldelev



Netherlands – Confidential site

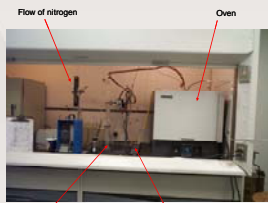
COC: Diesel (mass currently unknown)

Soil: Fractured limestone

Treatment depth: 6,5 meters

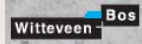
Area: 100 – 3.500 m²

Design based on treatability study – indicated remediation efficiencies better than 99.9% at treatment temperatures between 100 and 200 °C.



Flow of nitrogen Oven
Condensing system Temperature measurements

Test setup – laboratory experiments



Reerslev – Denmark

COC: PCE – 10.000 kg

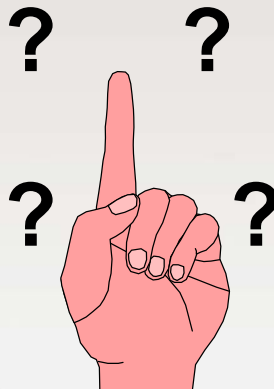
Soil: Clay

Treatment depth: 8 meters


Area: 900 – 4.700 m²




Thank you and:




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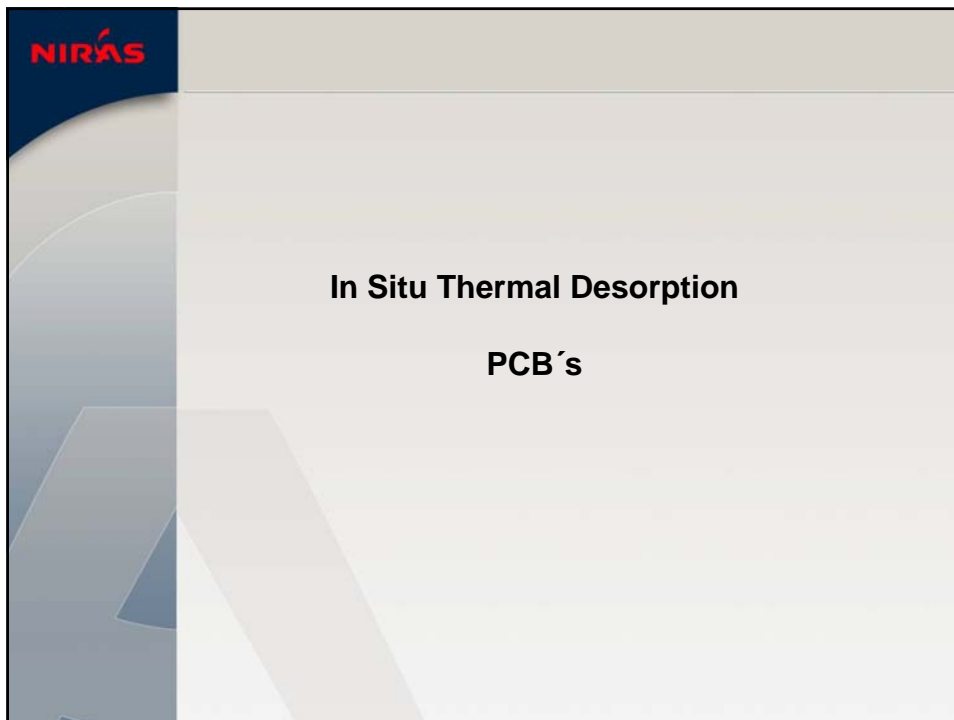
 Physical processes/changes (below 120 °C)						
Component property	Oil based LNAPL	Chlorinated solvents	Creosote	Coal tar	PCB	Comment
Vapor pressure increase factor	20-40	20-40	20-40	20-40	20-40	Abundance of data in literature
Solubility increase factor	2-100?	1.5-3	10-1000	10-1000	10-1000	Chlorinated solvent less affected than larger hydrocarbons
Henry's constant increase factors		10-20	0-10	0-10	0-10	Data absent for most compounds, some decrease?
Viscosity reduction factor	2 to 100+	1.3-3	5-10	20-100+	3-100	The higher initial viscosity, the more reduction
Interfacial tension reduction factor	<2	<2	2-5	1-5	<5	Typically not dramatic effect (less than factor 2)
Density reduction (%)	10-20	10-20	10-20	10-20	10-20	Note that DNAPL may become LNAPL
K _d (reduction factor)	?	1-10	5-100	5-100	NA	Estimates based on limited data

Udell (1989, 1991, 1993, 1996).
Davis (1997, 1999).
Imhoff et al. (1997).
Sleep and Ma (1997).
Heron et al. (1998, 2000).

 Energy consumption (kWh/m³)				
	Initial water content			
	100 %	80 %	10 %	0 %
Heating to 100 °C, wet	80	61	47	43
Heating to 100 °C & evaporating all porewater	299	171	69	43
Heating to 200 °C	347	219	117	91

 Target temperatures		
	VOC	SVOC
Above water table	90-100 °C (ERH, SEE, ISTD)	300 °C (ISTD)
Below water table	100-120 °C (ERH, SEE, ISTD)	100 -120 °C partial removal (ERH, SEE, ISTD low int.) 300 °C complete removal (ISTD, dewater)

ERH: Electrical Resistivity Heating
 SEE: Steam Enhanced Extraction
 ISTD: In Situ Thermal Desorption



Location	Contaminant	Initial Max. Concentration (ppm)	Final Concentration (ppm)
S. Glens Falls, NY	PCB 1248/1254	5,000	< 0.8
Cape Girardeau, MO	PCB 1260	20,000	< 0.033
Vallejo, CA	PCB 1254/1260	2,200	< 0.033
Saipan, NMI	PCB 1254/1260	10,000	< 1
Ferndale, CA	PCB 1254	800	< 0.17

Source: Stegemeier and Vinegar (2001)
Terratherm Inc.

ISTD

PAH's and Dioxins

